Hitachi Zosen INOVA

Hinwil / Switzerland Waste to Energy Plant



Kezo Hinwil Replaces Flue Gas Treatment System and Increases Energy Efficiency with New Effluent Free XeroSorp[®] Technology

The three flue gas treatment units at KEZO Hinwil installed in 1991 and 1995 used a combination of wet cleaning, effluent evaporation and SCR DeNOx, and were replaced in 2012 by two lines with Hitachi Zosen Inova's (HZI) new XeroSorp[®] process.

Pioneering the New Technology

Swiss thermal waste treatment plants previously relied on wet flue gas treatment (FGT) systems. Since no effluent discharge was possible at the Hinwil site, KEZO applied an energy consuming waste water evaporation. To improve its energy efficiency, KEZO took the lead by changing over to new technology using HZI's XeroSorp[®] process.

Stringent Requirements for the New Plant

The new effluent free system was designed to combine optimum energy efficiency with economically viable operation, while at the same time ensuring maximum availability and keeping emissions to a minimum, and, in so doing, to drive a technology change. Other reasons behind the decision to award the order to HZI included the little space required and the very short transition period.

Optimized Flue Gas Cleaning

The XeroSorp[®] process consists of a reactor, fabric filter, SCR DeNO_x, and heat exchanger. Flue gases from all three combustion lines are mixed together and then split between the two new, identical XeroSorp® lines. Sodium bicarbonate and lignite coke are injected into the flue gas as it enters the reactor. Static mixers in the XeroSorp® reactor ensure the mixing of the flue gas and the adsorption of acidic pollutants, heavy metals and dioxins. In the fabric filter, the solids form a filter cake. Solids collected in the filter bags are removed cyclically by pulse-jet cleaning. Most of the solids are recycled to the XeroSorp® reactor to achieve a very low excess ratio of unused additives. A part of the solids are extracted to the residue silo. The flue gases then pass without temperature change through an SCR $\mathsf{DeNO}_{\mathsf{x}}$ system, where nitrous oxides are reduced by injected ammonia. The low-temperature catalyst can be thermally regenerated while the system is in full operation with a low burner capacity. The cleaned flue gases then go through a heat exchanger for further energy recovery and are released by the stack.



Flue Gas Treatment

- 1 Adsorbent injection
- 2 Baghouse filter
- 3 Ammonia injection
- 4 Catalyst

Energy Recovery

9 Disctrict heating connection

Residue Handling and Treatment

- 10 Residue recirculation
- 11 Residue bunker
- 12 Residue discharge

An Idea Becomes Reality

The project at KEZO Hinwil started out ambitious in every respect, but even the high expectations were exceeded. Emissions are below the guaranteed level, operating costs are below expectations, and the unit was built with 60% less space required than a conventional FGT plant in just 15 months following the contract signature. The transition

5

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7 ID Fan

8 Stack

Regeneration burner

Heat exchanger

from the existing to the new flue gas treatment took less than 72 hours. An extra highlight is the increase in energy efficiency, with approx. 220 kWh more energy recoverd per ton of treated waste. The installation at KEZO Hinwil opened the way for further applications of this innovative technology.

Owner	KEZO Kehrichtverwertung Zürcher Oberland
Start of operation	2012 (New Flue gas treatment)
Investment	CHF 25 million
Scope of HZI	XeroSorp [®] Consists of reactor, fabric filter, SCR DeNO _v , heat exchanger, ID fan and stack
General contractor	Hitachi Zosen Inova
echnical Data	
Annual capacity	200,000 t
Number of lines	2 flue gas treatment
Waste type	Domestic and industrial waste
Concopt	H7I VaraCarp®
Concept	HZI XeroSorp®
Concept	HZI XeroSorp [®] Dry FGT with Sodiumbicarbonate and low temperature SCR DeNO _x with periodical catalyst activation, tail-end heat exchanger
Concept	HZI XeroSorp [®] Dry FGT with Sodiumbicarbonate and low temperature SCR DeNO _x with periodical catalyst activation, tail-end heat exchanger 87.000 Nm ³ /h
Concept Flue gas volume per line Flue gas temperature	 HZI XeroSorp[®] Dry FGT with Sodiumbicarbonate and low temperature SCR DeNO_x with periodical catalyst activation, tail-end heat exchanger 87,000 Nm³/h 190 °C, 120 °C at stack
Concept Flue gas volume per line Flue gas temperature Energy Recovery	 HZI XeroSorp[®] Dry FGT with Sodiumbicarbonate and low temperature SCR DeNO_x with periodical catalyst activation, tail-end heat exchanger 87,000 Nm³/h 190 °C, 120 °C at stack
Concept Flue gas volume per line Flue gas temperature Energy Recovery District heating	 HZI XeroSorp[®] Dry FGT with Sodiumbicarbonate and low temperature SCR DeNO_x with periodical catalyst activation, tail-end heat exchanger 87,000 Nm³/h 190 °C, 120 °C at stack 22,000 MWh/a (2013)
Concept Flue gas volume per line Flue gas temperature Energy Recovery District heating Greenhouse heating	 HZI XeroSorp® Dry FGT with Sodiumbicarbonate and low temperature SCR DeNO_x with periodical catalyst activation, tail-end heat exchanger 87,000 Nm³/h 190 °C, 120 °C at stack 22,000 MWh/a (2013) 20,000 MWh/a (2013)
Concept Flue gas volume per line Flue gas temperature Energy Recovery District heating Greenhouse heating Increase of thermal energy recovery with XeroSorp®	 HZI XeroSorp® Dry FGT with Sodiumbicarbonate and low temperature SCR DeNO_x with periodical catalyst activation, tail-end heat exchanger 87,000 Nm³/h 190 °C, 120 °C at stack 22,000 MWh/a (2013) 20,000 MWh/a (2013) +44'000 MWh/a
Concept Flue gas volume per line Flue gas temperature Energy Recovery District heating Greenhouse heating Increase of thermal energy recovery with XeroSorp® Residues	 HZI XeroSorp® Dry FGT with Sodiumbicarbonate and low temperature SCR DeNO_x with periodical catalyst activation, tail-end heat exchanger 87,000 Nm³/h 190 °C, 120 °C at stack 22,000 MWh/a (2013) 20,000 MWh/a (2013) +44'000 MWh/a